Cryogenic Moderator System Performance



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Moderator System Overview



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Target – Moderator Configuration





Hydrogen System Description

- The Hydrogen Moderator System is a series of three independent cryogenic loops each consisting of:
 - Moderator
 - load
 - transfer lines
 - Circulator
 - Flow control
 - Heat exchanger
 - Thermal control
 - Accumulator
 - Pressure control





Normal Operating Conditions

- The hydrogen system operates at supercritical conditions at all times to avoid phase change complications.
 - Minimum loop pressure is maintained at 14 bar.
 - Provides a 1 bar margin above the critical pressure.
- The system operates in a constant mass mode thus it must accommodate a certain degree of pressure perturbation resulting from frequent beam interruptions.
 - Beam off pressure ranges from 14 to 15 bar.
 - Circulator capable of a delivering a maximum of 1 bar differential.
 - Beam on pressure ranges from 15 to 16 bar.
- Hydrogen supply temperature is controlled to maintain an average moderator temperature of 20 K.
 - Temperature throughout the loop ranging from 17.5 K to 22.5 K.
- Heat exchangers are designed with a very tight approach.
 - 0.5 K



Pressure Control Philosophy

- Pressure is controlled passively by a cryogenic accumulator.
- The accumulator is a double walled design with an all stainless steel construction.
 - Helium backed bellows
- The accumulator vessel is actually surrounded by the flowing hydrogen.
 - Approaches isothermal expansion and compression of the helium.
 - Ensures adequate cool down.



Cryogenic Accumulator in "Action"



125 kW Beam Heating

 Refrigeration heater load response to beam heat indicates a nuclear load of ~300 W.

- ~2.4 W per 1 kW beam

- Hydrogen temperature is controlled within 0.25 K.
- Hydrogen pressure is controlled to within 0.6 psig.
- Pressure controlled passively by accumulator as recorded by ~2% shift in bellows position.



Helium Refrigerator Requirements

- The function of the Helium Refrigerator is to cool these three parallel-connected hydrogen loops and subsequently maintain a nominal hydrogen supply temperature of 17 K from each heat exchanger against a continuous combined heat load of 7.5 kW.
- As such, the vendor was given responsibility for the design and fabrication of all helium bearing components.
- Temperature control was specified at +/- 0.5 K.
- To meet this requirement, the vendor specified hydrogen-to-helium heat exchangers with a 0.5 K approach.
 - This resulted in a a required 16.5 K helium supply temperature.



Helium Refrigerator Commissioning

- When the system was originally commissioned in January 2005, it failed its performance test.
 - The system was unable to attain its specified 7.5 kW @ 16.5K.
 - Not only did it come short of its capacity goal, it could not operate stably at design conditions
 - 40 psig compressor suction
 - Apparent stable operation was ultimately achieved at a lower suction pressure of 20 psig
- At that time, it appeared that the system would operate sufficiently for a long period of time but at a greatly reduced capacity
 - Capacity was still sufficient to support operations in excess of 1MW.
- In fear of jeopardizing CD-4, the decision was made to postpone any repair attempts.



Helium Refrigerator Operation

 Early in operations, however, it was discovered that the system mysteriously suffered from a steady decline in cooling capacity.





Contamination?

- Air Liquide's first suspicion was contamination.
 - Water
 - Air
 - Oil
- A number of tests and analyses were performed and it was concluded that the system was clean and dry.
- During the testing phase, operation at design conditions would result in a rapid decay.
- Lowering the suction pressure, however, appeared to allow the system to recover.
 - This was inconsistent with the assumption that the heat exchanger was fouling due to contamination.



Flow-Induced Mal-distribution?

- Two openings were made along the length of the cold box to allow for access to the heat exchanger.
 - RTD's were attached across the height of the heat exchanger at these two locations.
 - RTD readings were logged during subsequent production runs.
- These readings clearly showed that the top of the heat exchanger was warmer than the bottom.
- It was also clear that the heat exchanger was becoming progressively shorter as a function of time.
 - 90K only 1 foot from the cold end operating at ~30K!
- These results coupled with analysis performed by Air Liquide, lead to the conclusion that the heat exchanger was suffering from a propagating mal-distribution perhaps caused by small pressure drop in the core.
 - The pressure drop is significantly reduced by the fact that the flow in the channels is actually laminar as opposed to turbulent.



Helium Refrigerator Modifications

- After presenting their analysis to SNS Management, it was agreed that the heat exchanger should be removed and perforated plates be installed into each of the headers.
- This work was performed during the '06 Christmas outage.
 - The heat exchanger was extracted, shipped to CHART for repair, re-installed, and the system operational before the end of the outage.
- Initial indications were promising as the system appeared to operate stably at design conditions for a period of 4 days.
 - Before the modification, operation at design conditions resulted in a noticeable decay in performance within 45 minutes.
- Continued operation of the system, however, during the following cycle revealed the fact that the system continued to suffer from a slow degradation in capacity.



Contamination, again?

- After the header modifications only resulted in a decrease in the rate of performance degradation, Air Liquide once again turned to contamination as an explanation and initiated a new battery of tests:
 - Compressor oil samples were analyzed.
 - HX was isolated at the conclusion of a production run, and pumped down through a LN2 cold trap.
 - Negligible quantity of water found.
 - Consolidated Science performed detailed on-site analysis of the helium both in the process stream as well as the buffer tank.
 - 17 ppm of Nitrogen found in the buffer tank helium.
- At the conclusion of these tests, Air Liquide suggested that the helium be purified by operating the refrigerator for several brief periods between which the adsorber was regenerated.
 - At the conclusion of the purification process, the buffer tank nitrogen concentration was down to ~2 ppm.
 - During subsequent operation of the refrigerator, the rate of decay was unaffected.



Tower Water Instability?

- Quickly running out of theories, our attention turned to the noticeably noisy warm end temperature differentials.
- The after cooler on the compressor skid was cooled using the site's tower water facility.
 - The temperature control for this system is rather poor resulting in large temperature swings that correspond to when the cooling water fans cycle.
- This instability in tower water transmitted its fluctuations directly into the helium stream entering the high pressure header on the warm end of the heat exchanger.
- Operational experience during the winter months indicated a system preference to cool weather which coincidentally corresponded to periods of more stable tower water temperature.
- The tower water cooling circuit was disconnected from the after cooler and was replaced by a more stable chilled water cooling circuit.
- While noticeably smoothing the warm end temperature differentials, the rate of decay was seemingly unaffected but did yield some additional cooling capacity.



Impacts on Future Operation

- Our current mode of operation was unacceptable.
 - ~20 day run cycles were resulting in frequent cycling of components and equipment.
- If the beam ramp up schedule is met, SNS will be operating at 1.4 MW by October 2009.
- At 1.4 MW, the refrigeration system will be able to accommodate cold neutron production for ~6 days continuously before it will be required to be warmed.
 - Each warm up / cool down cycle requires 3 days.
- There is no way SNS can meet its beam availability goal of >90% with a refrigeration system that can only provide at best 66% availability.
 - Not to mention that with the excessive number of thermal cycles, something WILL break eventually.



External Advisory Committee

- With no clear path forward, an external advisory committee was formed.
- The committee recommended that we "develop a short term fix that would provide more stable capacity for the short term, and an appropriate fix for the long term."
- To that end, we procured two replacement HX's that would have been installed this summer to addresses the long term.
 - The design of this replacement pair of HX's are based on the operating experience of a similar but stably operating Air Liquide facility.
- While waiting for our new HX's, we faced the prospect of progressively shorter refrigerator run cycles resulting from the expected ramp up in beam power.
- Our attention then turned to developing a short term fix.



Self-propagating Mal-Distribution Causes

- We had investigated a number of potential causes for a selfpropagating mal-distribution.
- The two causes that remained were:
 - Manufacturing defects in the HX that results in a significant nonuniformity of channel cross section areas,
 - Temperature gradient across the stack height as the result of HX's horizontal orientation.
- Recent experience at the WTRF in Korea, however, indicated an almost identical slow degradation of the refrigeration system's performance over time.
 - This implied a low probability that the cause was a manufacturing defect, as the two HX's were manufactured by different companies.
- This left us with gravity-driven mal-distribution.
 - The ILL refrigeration system consists of one HX block with NO LN2 pre-cooling and has been operating in a stable manner since the 70's.
 - The HX, however, is oriented vertically.



Short-term Fix Proposal

- Last Christmas we demonstrated the ability to extract the HX, ship it to CHART for repair, re-install the HX, and leak test in a period of one month.
- The proposal involved once again extracting the HX but to install it into a new vertically oriented auxiliary vacuum enclosure to be located at the cold end of the existing cold box.
- The HX would be extracted by the same team that performed this work previously.
- The HX would then be shipped to AET for installation into the new box while work would proceed on site preparing the new piping connections.
- The new auxiliary vacuum enclosure would need only accommodate 4 single walled piping connections.
 - Warm piping would by-pass the existing cold box externally
 - Cold piping connections would be made via a 24" access port



HX Re-orientation Schedule of Events

- The extraction process started on October 4.
- HX shipped to AET on October 7.
 - Oil found in process piping at AET on October 10.
 - Sent to Consolidated Science for Analysis.
 - Control sample of our compressor oil sent for comparison
 - Analysis repeated by Consolidated confirms presence of compressor oil in cold box piping.
- Witch's hat inspected on October 22.
 - Presence of charcoal and oil indicate failure of the Oil Removal System.
 - Oil Removal System Rebuild started on October 24.
- Methanol flushing of process piping began on October 26.
- The new cold box arrived on October 31.
- Refrigerator was re-started on November 5.





















Operational Experience to Date

Vertical HX First Neutron Production Run



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Cryogenic Moderator System Performance

Summary

- Accumulator-based pressure control system has been successful at passively controlling the loop pressure of a circulating supercritical hydrogen loop.
 - Projections indicate that the system will be able to accommodate full beam power at 1.4 MW.
- Despite suffering from a capacity degradation, the helium refrigeration system has been successful at controlling the hydrogen circuits to within +/- 0.5 K.
- Re-orientation of the HX from horizontal to vertical has proven successful.
 - Operation of the refrigerator at design conditions is projected to yield ~8 kW of cooling.

